USS ANCHORAGE LSD 36 PROPULSION OPERATING GUIDE



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LONG BEACH NAVAL SHIPYARD LONG BEACH, CALIFORNIA

NAVAL SEA SYSTEMS COMMAND

NAVY DEPARTMENT

THIS BOOKLET IS INTENDED TO SERVE ENGINEERING PERSONNEL AS A PERFORMANCE STANDARD IN DESCRIBING THE DESIGN FUNCTIONS OF THE MAIN AND AUX PROPULSION SYSTEMS AND MAY BE USED FOR MONITORING OPERATING CONDITIONS OF THOSE SYSTEMS. RATINGS AND DATA HAVE BEEN SELECTED FROM DESIGN HEAT BALANCE CALCULATIONS, PERFORMANCE CHARCTERISTICS OF INDIVIDUAL EQUIPMENT, AND MANUFACTURERS TECHNICAL MANUALS. SYSTEM DIAGRAMS AND MACHINERY ARRANGEMENT SKETCHES WERE DERIVED FROM INGALLS SHIPBUILDING DIV, LITTON SYSTEMS PLANS AND MODIFIED BY SHIPALT AND OTHER SYSTEM CHANGES. PROPULSION SYSTEM OPERATING, SAFETY AND MAINTENANCE NOTES WERE DERIVED FROM REFFERENCED AND THIS BOOKLET SHOULD BE THOROUGHLY STUDIED SINCE PROPER OPERATION AND MAINTENANCE WILL ENSURE SAFE AND EFFICIENT OPERATION OF THE PROPULSION SYSTEMS. FOR ADDITIONAL DATA AND DETAILED OPERATIONAL MAINTENANCE WILL ENSURE SAFE AND EFFICIENT OPERATION OF THE PROPULSION SYSTEMS. FOR ADDITIONAL DATA AND DETAILED OPERATIONAL AND PLANS FURNISHED THE SHIP AND THE FOLLOWING TECHNICAL MANUALS:

COMPRESSED AIR PLANTS	GEARS. ND SEALS. LEMENT) IANGERS & AIR EJEC S. S. S. S. D. EQUIPMENT. R. TEST & TREATM APPARATUS. SENERAL LERATORS. LIBUTION SYSTEM. CONTROLLERS. CONTROLLERS.	OLD NEW 9411 231 9412 233 9420 241 9450 243 9450 243 9450 244 9450 254 9470 503 9470 503 9480 254 9470 503 9480 505 9500 502 9510 221 9530 554 9550 541 TMENT 9560 220 9562 255 9580-1 531 9600 300 9610 310 9621 320 9630 502	LUBE OIL SERVICE PUMPS. DISTILLER BRINE OVBD DISCHARGE PUMP. FUEL OIL TRANSFER PUMP. MN. CONDENSTATE PUMP. MAIN FEED PUMP (TD). FUEL OIL SERVICE PUMP (TD). MAIN GIRCULATING PUMP. MAIN CIRCULATING PUMP. DISTILLER DISTILLATE PUMP. 1000 GPM FIRE PUMP (TD). 500 GPM FIRE PUMP (TD). 500 GPM FIRE PUMP (TD). COMPRESSOR. MAIN BOILERS. AUTO. COMB. AND FDW CONTROLS FOR MAIN BOILERS. FORCED DRAFT BLOWERS. DEAERATING FEED TANK.	NAVSEA NO. 0941-028-1010 0945-005-9010 0947-083-3010 0947-083-3010 0947-128-3010 0947-123-0010 0947-123-0010 0947-124-0010 0947-124-3010 0947-124-4010 0947-131-5010 0947-131-8010 0947-131-8010 0947-131-8010 0947-131-8010 0947-131-8010 0947-131-8010 0947-131-8010 0947-131-8010 0947-131-8010 0947-131-9010 0947-132-0010 0947-132-0010 0947-132-0010 0947-132-0010 0947-132-0010 0947-132-0010 0947-132-0010 0947-132-0010 0947-132-0010 0947-132-0010
FORCED DRAFT BLOWERS			FORCED DRAFT BLOWERS. DEAERATING FEED TANK. 30.000 G.P.D. FLASH TYPE DISTILLING PLANT	0953-011-5010 0956-014-6010 0358-038-4000

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OPERATING NOTES FOR NAVY FUELS

- *1. FUELS FOR USE FOR SURFACE FOSSIL FUELED SHIPS SPECIFIED BY OPNAV INSTRUCTION 9550.4A ARE LISTED BELOW IN ORDER OF PRE-
 - A. DIESEL FUEL MARINE (DFM) MIL-F-16884G, NATO SYMBOL F-76.
 - B. ACCEPTABLE ALTERNATE FUELS (LISTED IN PRIORITY ORDER AND COMPATIBLE IN ANY PROPORTION).
 - (1) JP-5, MIL-T-5624, (NATO SYMBOL F-44).
 (2) NATO SYMBOL F-75
 (AS AVAILABLE FROM NATO COUNTRIES).

 - (AS AVAILABLE FROM NATIONAL CONNINTED;

 (AS TAVAILABLE FROM NATIONAL CONNINTED;

 F. 54, PROVIDING THE FLASH POINT IS 140°F OR ABOVE.

 (4) AS TM-D-975 NO. 2-D, PROVIDING THE FLASH POINT IS 140°F OR ABOVE.
- II. THE SPECIFICATION HEAT CONTENT IS 19,500 BTU/LB. FOR ALL DISTILATES (ND, DIESEL, JP-5). THE SPECIFICATION DENSITY IS 7.0 LB/GAL. FOR DIESEL AND 6.8 FOR JP-5.
- III.THE STRAIGHT MECHANICAL BURNER SYSTEM WHEN OPERATING WITH DISTILLATE FUEL REQUIRES THE SPRAYER PLATE SIZE SHOWN ON PAGE 22.

WHEN BURNING DISTILLATE FUELS, A HAZE (STACK CONDITION) SHOULD NOT BE USED. PROPER COMBUSTION IS BEST ATTAINED BY LOWERING AIR PRESSURE UNTIL A LIGHT HAZE APPEARS IN THE STACK AND THEN RAISING BLOWER SPEED SLIGHTLY UNTIL A CLEAR STACK APPEARS.

IV. FUEL OIL SERVICE TANKS

SHIFT FUEL OIL SERVICE TANKS WHEN TANK IN SERVICE REACHES 50% LEVEL TO ENSURE AN ADEQUATE GRAVITY HEAD FOR THE FUEL OIL SERVICE PUMP.

V. FUEL OIL TESTING - TAKE SAMPLES AND MEASURE B.S.&W. (USE LIMIT-.1% OF FUEL TANKS AS FOLLOWS:

ALL TANKS - AT LEAST ONCE EACH WEEK STORAGE TANKS - 24 HOURS AFTER RECEIPT AND PRIOR TO TRANSFER SERVICE TANKS - PRIOR TO PLACING ON SUCTION

- VI. TUBE BLOWING PROCEDURE
 - A. WHILE UNDERWAY, IN PORT, OR AT ANCHOR, THOROUGHLY BLOW TUBES IN ALL STEAMING BOILERS AT LEAST ONCE

 - B. ALWAYS THOROUGHLY BLOW TUBES AFTER LEAVING OR JUST PRIOR TO ENTERING PORT.
 C. WHEN PRACTICAL, THOROUGHLY BLOW TUBES JUST AFTER THE MAKING OF HEAVY SMOKE FROM ANY CAUSE (LIGHTING OFF, CASUALTY, ETC.).

*NOTE: ABOVE FUELS AUTHORIZED FOR NAVY USE AT TIME OF PUBLICATION OF THIS POG. FOR EMERGENCY SUBSTITUTE FUELS AND DETAILED OPERATING PROCEDURES SEE OPNAV INSTRUCTION 9550.4A NAVSEA TM CHAPTER 541 (PETROLE-UM FUEL STOWAGE, USE AND TESTING) AND NAVY DISTILLATE (ND) CONVERSION PROGRAM ACQUISITION MASTER PLAN VOLUMES I AND II AND PERTINENT ND ADVISORIES.

	RATINGS	FOR	PROPULSION	UNITS
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MAIN TURBINE	
MANUFACTURER:	DELAVAL TURBINE, INC
2 INSTALLED:	CROSS COMPOUND IMPULSE TYPE
	H ASTERN ELEMENTS IN LP STAGE
24,000	SHP PER SHIP AHEAD AT 235 PRPM
12,000	SHP PER UNIT AHEAD AT 235 PRPM
4,800	SHP PER SHIP ASTERN AT 130 PRPA
2,400	SHP PER UNIT ASTERN AT 130 PRMF

DESIGN CONDITIONS: (FULL POWER)

THROTTLE STEAM PRESSURE - 585 PSIG
THROTTLE STEAM TEMPERATURE - 850° F
CONDENSER PRESSURE - 2.0 IN H_g ABSOLUTE

MAIN REDUCTION GEAR

MANUFACTURER: DE LAVAL TURBINE, INC
2 INSTALLED: DOUBLE HELICAL, ARTICULATED, DOUBLE
REDUCTION TYPE

HP TURBINE REDUCTION - 7637/235
LP TURBINE REDUCTION - 5298/235

MAIN CONDENSER

MANUFACTURER: INDUSTRIAL PROD. DIV. MARYLAND SHIPBLDG. .

§ DRYDOCK CO.

2 INSTALLED PER SHIP, SINGLE PASS ARRANGED ATHWARTSHIP SURFACE AREA - 6300 SQUARE FEET

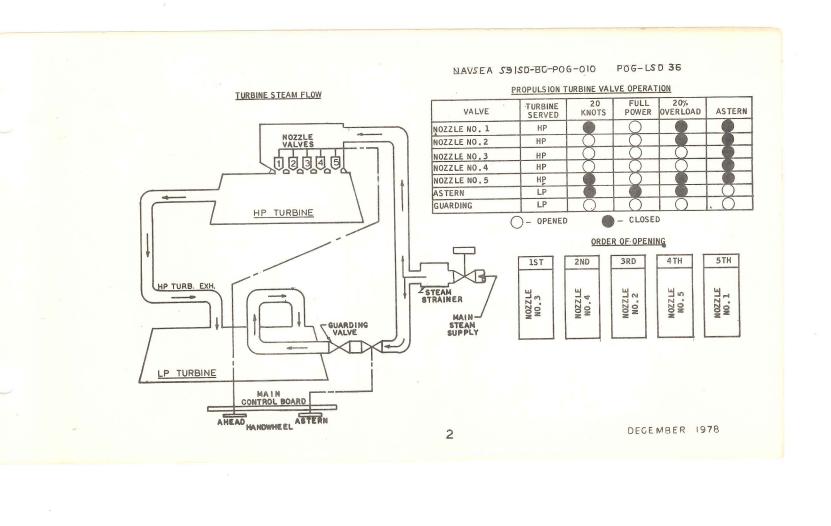
DESIGN CONDITIONS - FULL POWER

STEAM CONDENSED (LB/HR)	77,280
ABS. PRESSURE AT CONDENSER INLET (IN. HG.)	2.0
INLET WATER TEMPERATURE (°F)	75
OUTLET WATER TEMPERATURE (°F)	83.6
CIRCULATING WATER QUANTITY (GPM)	17,000
AUXILIARY EXHAUST STEAM (LB/HR)	6,000

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(PGIC)	13
DESIGN STEAM OPERATING PRESSURE (PSIG)	450
STEAM TEMPERATURE TO AIR EJECTOR (°F)	45
STEAM CONSUMPTION ~	
FIRST STAGE NOZZLE (LB/HR)	15
SECOND STAGE NOZZLE (LB/HR)	120
FREE AIR REMOVAL CAPACITY PER ELEMENT (LB/HR)	22.
	1.0
	71.
	16
COOLING WATER INLET TEMPERATURE (OF)	79.
COOLING WATER OUTLET TEMPERATURE (°F)	20.
COOLING WATER PRESSURE DROP (PSI @165 GPM)	1.
COOLING WATER PRESSURE DROP (PSI &103 GFM)	

WANUFACTURER: BETHLEHEM STEEL CO.
2 PER SHIP: 1 RH (STBD) AND 1 LH (PORT)
5 BLADE, MANGANESE BRONZE
DIAMETER - 12 FEET 6 INCHES
PITCH - 11 FEET 10-5/8 INCHES AT 0.7R



BOILER PERFORMANCE DATA

MANUFACTURER: COMBUSTION ENGINEERING INC.

7 PER SHIP. "D" TYPE STEAM GENERATORS, FUEL OIL
FIRED, TWO DRUM, SINGLE FURNACE, INTEGRAL SUPERHEATER,
FORCED DRAFT TYPE, WITH ECONOMIZER, SOOT BLOWERS,
AND WATER DRUM INSTALLED DESUPERHEATER

OPERATING PRESSURES AND TEMPERATURES

DESIGN PRESSURE 710 PSIG
STEAM DRUM PRESSURE 660 PSIG (FULL POWER)
SUPERHEATER OUTLET PRESSURE 660 PSIG (F.P.)
SUPERHEATER OUTLET TEMPERATURE 850°F
DESUPERHEATER OUTLET TEMPERATURE 570 PSIG (F.P.)
600 CRUISING
DESUPERHEATER STEAM OUTLET TEMPERATURE 580°F (F.P.)
ECONOMIZER INLET TEMPERATURE 241°F
ECONOMIZER OUTLET TEMPERATURE 355°F (F.P.)
350°F (CRUISING)

BOILER SAFETY VALVES POPPING (PSIG) RESEATING (PSIG	
DRUM PILOT ACTUATOR 710 685	
SUPERHEATER 725 700	
DRUM VALVE NO. 1 725 700	
DRUM VALVE NO. 2 735 710	

BURNERS

LERS
MANUFACTURER: TODD SHIPYARDS CORPORATION
THREE INSTALLED PER BOILER, RETURN FLOW, MECHANICAL
PRESSURE ATOMZIING, MODEL D-17, WITH CONSTANT SUPPLY
PRESSURE AND VARIABLE RETURN PRESSURE.

AUTOMATIC COMBUSTION CONTROL

MANUFACTURER: HAGAN CONTROLS CORPORATION
ONE SYSTEM INSTALLED PER BOILER TO MAINTAIN PROPER
COMBUSTION BY REMOTE MANUAL OR AUTOMATIC REGULATION
OF FUEL OIL AND AIR REQUIREMENTS.

AUTOMATIC THREE ELEMENT FEEDWATER REGULATOR SYSTEM
MANUFACTURER: HAGAN CONTROLS CORPORATION
ONE SYSTEM IS INSTALLED PER BOILER TO MAINTAIN SAFE
WATER LEVEL IN STEAM DRUM BY SENSING FEEDWATER FLOW,
STEAM FLOW AND STEAM DRUM WATER LEVEL.

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THE FOLLOWING DESCRIPTION RELATES TO ONE TURBINE SET; IT CAN BE ASSUMED THAT OPERATION OF BOTH MAIN TURBINE SETS IS IDENTICAL.

AHEAD OPERATION IS ACCOMPLISHED BY A SINGLE HANDWHEEL OPERATING THE AHEAD NOZZLE THROTTLE VALVES THROUGH A CAM LIFTING MECHANISM. DURING AHEAD OPERATION THE ASTERN VALVE SHOULD BE VERIFIED CLOSED.

ASTERN OPERATION IS ACCOMPLISHED BY A SINGLE HANDWHEEL OPERATING THE ASTERN THROTTLE VALVE. GUARDING VALVE IN STEAM LINE TO ASTERN TURBINE MUST ALSO BE CHECKED OPEN. DURING ASTERN OPERATION THE AHEAD NOZZLE THROTTLE VALVES SHOULD BE VERIFIED CLOSED.

BEFORE TURNING THE PROPULSION TURBINE, CHECK THE LUBE OIL TEMPERATURE. IF IT IS BELOW 90 DEGREES F, HEAT THE OIL TO THAT TEMPERATURE BY RECIRCULATING IT THROUGH THE LUBE OIL PURIFIER HEATER. DO NOT OPERATE THE TURBINES WITH A LUBE OIL TEMPERATURE BELOW 90 DEGREES F, EXCEPT IN AN EMERGENCY. DURING NORMAL OPERATION THE TEMPERATURE OF THE SUPPLY LUBE OIL SHOULD BE APPROXIMATELY 1209/130°F. THE MAXIMUM TEMPERATURE RISE OF LUBE OIL PASSING THROUGH ANY BEARING, UNDER ANY OPERATING CONDITION, SHALL NOT EXCEED 50°F NOR SHOULD THE FINAL TEMPERATURE OF THE LUBE OIL AT OUTLET OF ANY BEARING EXCEED 180°F.

WITH LUBE OIL SYSTEM OPERATING, ENGAGE THE TURNING GEAR AND ADMIT SEALING STEAM TO WARM-UP TURBINE ROTORS. WHEN TURBINE ROTOR WARM-UP IS COMPLETED DISENGAGE THE TURNING GEAR AND ADMIT ASTERN AND AHEAD THROTTLE STEAM ALTERNATELY TO SPIN THE TURBINES. DO NOT PUT WAY ON THE SHIP WHILE SPINNING. BE ATTENTIVE TO ANY RUBBING SOUND OR UNDUE NOISE AND IF ANY IS DETECTED, SECURE THROTTLE STEAM AND CORRECT THE CALISF.

TURBINE ROTORS SHOULD NOT BE PERMITTED TO REMAIN STATIONARY FOR LONGER THAN 3 MINUTES WITH STEAM ENTERING THE TURBINE FROM ANY SOURCE. FOR PROLONGED STANDBY CONDITION, ROTATE TURBINE ROTORS BY MEANS OF THE TURNING GEAR.

ALL TRAPPED TURBINE DRAINS SHOULD REMAIN OPEN DURING TURBINE OPERATION. HOWEVER, ALL UNTRAPPED TURBINE DRAINS TERMINATING IN THE CON-DENSER SHOULD BE CLOSED DURING NORMAL OPERATION. THEREFORE, ANY UNTRAPPED TURBINE DRAINS KEPT IN OPEN POSITION TO FACILITATE STANDBY OR EXTENDED MANEUVERING OPERATIONS SHOULD BE OBSERVED CLOSELY FOR EFFECT ON VACUUM AND CONDENSING EQUIPMENT, AND SHOULD BE CLOSED IMMEDIATELY WHEN THEIR SERVICE OPERATION IS COMPLETED.

UNDER NO CIRCUMSTANCE SHOULD THROTTLE STEAM BE ADMITTED TO THE TURBINES WHEN THE TURNING GEAR IS ENGAGED.

NOTES ON BOILER OPERATION

IN ORDER TO OBTAIN MAXIMUM EFFICIENCY FROM THE STEAM GENERATING EQUIPMENT AND SUPPORTING AUXILIARIES, IT IS MANDATORY THAT ALL OPERATING PERSONNEL BECOME FAMILIAR WITH THE FOLLOWING APPROVED OPERATING AND MAINTENANCE PROCEDURES:

THE NORMAL WATER LEVEL IS AT THE HORIZONTAL CENTERLINE OF THE STEAM DRUM. THE LEVEL SHOULD BE HELD AS CLOSE TO THIS POINT AS POSSIBLE. IT IS IMPORTANT NEVER TO ALLOW THE LEVEL TO GO ABOVE THE TOP OF THE UPPER GAGE GLASS. TO KEEP THE LEVEL FROM RISING TOO HIGH, SHUT OFF THE FEEDWATER; AND, IN CASES OF EMERGENCY, OPEN THE SURFACE BLOWDOWN VALVE.

IN CASE OF HIGH OR LOW WATER LEVELS, EXCEPT FOR MOMENTARY FLUCTUATIONS DURING RAPID MANEUVERING, WHENEVER THE WATER DISAPPEARS FROM SIGHT (EITHER HIGH OR LOW):

- 1. SECURE OIL SUPPLY TO ALL BURNERS.
- 2. OPEN SUPERHEATER OUTLET HEADER DRAIN VALVE TO VENT THE SUPERHEATER BY MAINTAINING STEAM FLOW.
- 3. CLOSE FEED-CHECK VALVES.
- 4. CLOSE BOILER STEAM STOP VALVES.
- 5. IF THERE IS ANY QUESTION AS TO WHETHER THE CONDITION IS HIGH WATER OR LOW WATER, BLOW THROUGH WATER GAGES TO DETERMINE DEFINITELY WHETHER GAGES ARE FULL OR EMPTY.
- 6. IN EVENT OF HIGH WATER, BLOW THE BOILER DOWN TO THE MIDDLE OF THE GAGE GLASS BY USING THE SURFACE BLOW VALVE. RELIGHT BURNERS AS
- 7. IN THE EVENT OF LOW WATER, OPEN SAFETY VALVES CAUTIOUSLY BY HAND AND RELIEVE BOILER PRESSURE GRADUALLY.
- 8. CLOSE BURNER REGISTERS AND DIMINISH AIR SUPPLY TO THE BOILER BY STOPPING THE BLOWERS.
- 9. IN THE EVENT OF LOW WATER, IT IS ESSENTIAL THAT NO ATTEMPT BE MADE TO RESTORE NORMAL WATER LEVEL IN ANY MANNER THAT WOULD RESULT IN SUDDEN AND TOO RAPID COOLING OF OVERHEATED PRESSURE PARTS.

NOTES ON BOILER OPERATION (CONT'D)

LOW WATER IS THE MOST DANGEROUS CONDITION EXPERIENCED IN THE OPERATING OF STEAM GENERATORS, AND IS GENERALLY DUE TO INATTENTION ON THE PART OF THE OPERATORS. IF THE LOSS IS GRADUAL AND NOTICED BY THE OPERATORS:

- 1. INCREASE THE RATE OF FEED.
- 2. CHECK FEED LINE FOR LEAKS OR PARTIALLY CLOSED VALVES.
- 3. CHECK BLOW DRAIN AND VENT VALVES FOR LEAKS OR OPENED VALVES.
- 4. CHECK AUXILIARIES FOR WATER IN STEAM FROM AUXILIARY STEAM LINE WHICH INDICATES LEAKAGE FROM BOILER WATER DRUM INTO DESUPERHEATER.
- 5. START AUXILIARY FEED SYSTEM.

OPERATING WITH MARINE DIESEL FUEL OPERATE THE SOOT BLOWERS AT LEASE ONCE PER WEEK WHILE UNDERWAY, IN PORT, OR AT ANCHOR TO THOROUGHLY BLOW TUBES IN ALL STEAMING BOILERS. ALWAYS THOROUGHLY BLOW TUBES AFTER LEAVING OR JUST PRIOR TO ENTERING PORT. WHEN PRACTICAL, THOROUGHLY BLOW TUBES JUST AFTER THE MAKING OF HEAVY SMOKE FROM ANY CAUSE (LIGHTING-OFF), CASUALTY, ETC.). IT IS MANDATORY THAT THE BOILERS BE FIRED DURING ANY SOOT BLOWER OPERATION.

WHEN LIGHTING OFF, THE FUEL OIL SERVICE DISCHARGE HEADER PRESSURE SHOULD BE 400 PSIG AND THE COMBUSTION CONTROL SYSTEM SHOULD BE OPERATED ON "MANUAL". BRING BOILER PRESSURE UP TO PRESSURE WITH ONE BURNER IN USE AND COMBUSTION CONTROL SYSTEM ON "REMOTE MANUAL". DO NOT PERMIT SUPERHEATER OUTLET TEMPERATURE TO EXCEED 850°F. IT SHOULD BE NOTED THAT THE WATER LEVEL IN THE STEAM DRUM WILL RISE AS THE BOILER IS BROUGHT UP TO PRESSURE; IN THIS CASE, REDUCE RATE OF FEED OR OPERATE SURFACE BLOW VALVE TO LIMIT THE WATER LEVEL RISE TO 5 IN.(MAX.) ABOVE NORMAL WATER LEVEL.

THE BOILER OPERATING CONDITIONS DESCRIBED ON THE FOLLOWING PAGES ARE FOR ECONOMICAL STEADY STATE STEAMING CONDITIONS. FOR MANEUVERING, ALL BURNERS AND MAIN FORCED BLOWERS SERVING STEAMING BOILERS SHOULD BE IN OPERATION.

NOTES ON AUXILIARY MACHINERY OPERATION

THE OPERATION OF AUXILIARY MACHINERY SHALL BE IN ACCORDANCE WITH TECHNICAL MANUAL'S APPLICABLE TO THE SPECIFIC EQUIPMENT. ALL SAFETY PRECAUTIONS CONTAINED IN TECHNICAL MANUALS AND AS POSTED AT EQUIPMENT LOCATIONS SHALL BE STRICTLY ENFORCED IN ORDER TO OBVIATE POSSIBILITY OF INJURY TO PERSONNEL AND DAMAGE TO EQUIPMENT.

WHEN WARMING UP THE TURBO-GENERATORS, BE ATTENTIVE FOR ANY RUBBING OR OTHER UNDUE NOISE. CHECK FOR PROPER OIL FLOW AND BEARING TEMPERATURES, PROPER GLAND SEALING STEAM FLOW AND FOR EASE OF OPERATION. TURBINE ROTORS SHOULD NOT BE PERMITTED TO REMAIN STATIONARY FOR LONGER THAN THREE MINUTES WITH STEAM ENTERING THE TURBINE FROM ANY SOURCE.

BEFORE STARTING ANY PUMP, VERIFY THAT THE SUCTION LINE AND PUMP CASING HAVE BEEN FLOODED WITH SYSTEM FLUID. PUMPS FITTED WITH PRIMERS SHALL BE PRIMED AS REQUIRED. SOME PUMPS ARE LUBRICATED BY THE SYSTEM FLUID. THEREFORE, IT IS MANDATORY THAT THE FAILURE OF ANY PUMP TO MAINTAIN PROPER DISCHARGE, BE INVESTIGATED AND CORRECTED.

WARNING: TO ELIMINATE POTENTIAL HAZARDS WITH COMPRESSED AIR SYSTEMS COMPLY WITH THE FOLLOWING PROCEDURES:

- 1. ALL AIR DRYERS AND FILTERS SHALL BE MAINTAINED CLEAN AND IN GOOD WORKING ORDER.
- 2. AIR FLASKS, MOISTURE SEPARATORS AND LOW SPOTS IN PIPING SYSTEM SHALL BE PURGED FREQUENTLY TO ELIMINATE WATER AND OIL.
- 3. COMPRESS OR AIR INTAKE FILTERS SHALL BE KEPT CLEAN AND CARE SHALL BE EXERCISED TO ENSURE THAT THE AIR INTAKE IS NOT OBSTRUCTED WITH CLOTHING, RAGS, DEBRIS, ETC.
- 4. FOLLOW INSTRUCTIONS OF CHAPTER 551 OF NAVAL SHIPS TECHNICAL MANUAL.

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POG-LSD	36

	NO. PER SHIP DRIVE GPM			DISCH PRESS	SUCTION	PUMP		MOTOR	REMARKS
FRESH WATER PUMPS		PSIG	LIFT.	RPM ·	BHP	HP	KEMAKKS		
OTABLE WATER	2	М	125	60	FLOODED	35.50	7	10	
UST. DISTILLATE	2	М	30	35	FLOODED	3500	1.75	3	

	NO. PER		3	DISCH PRES	SUCTION		PUMP	MOTOR	
		DRIVE	GPM	PSIG	LIFT	RPM	BHP	HP	REMARKS
SEA WATER PUMPS BILGE	2	М	2500	11.48	3 FT	8,00	62.5	7.5	
MN COND CIRC CIRC	1 4	141	7600	5.80			40.8		
SSTG COND CIRC	4	М	950	20.	FLOODED	1750	13	15	
DIST. FEED PUMP	2	М	430	35	FLOODED	1760	11.1	15	
DIST. BRINE OVBD	2	М	410	30	27" HG	1175	12.0	15	
AUX. MCHRV SW CIRC	2	М	300	50	FLOODED	3535	12	15	
FIRE PUMP	4	M	500	150	FLOODED	3500		100	
FIRE PUMP	2 1	T M	1000 1000	150 150	FLOODED FLOODED	3500 3500		125	4930 LB/HR ST.

RATINGS OF AUXILIARY MACHINERY

OIL PUMPS & PURIFIERS	NO. PER	DRIVE		DISCH: PRESS PSIG	SUCTION LIFT	RPM . P	UMP BHP	MOTOR HP	REMARKS
MAIN F.O. SERVICE	4	T	21	400	5" HG	2020	8.3		
PORT USE F.O. SERV.	2	М	14/5	400.	15/20"HG	3500/1750	10/3.6	10/5	
F.O. TRANSFER	2.	М	250/500	150	15/20	850/1750	57.5	1	
BILGE AND F.O. TANK STRIPPING	2	RECIP	100	50	12" HG	6"x17"x12"- PISTON-22 F			340 LBS/HR STEAM FLOW
L. OIL PURIFIER	2	М	225 GPH	25	20" HG	1800		1.5	
L.O. SERV NORMAL (STANDBY) WARM-UP	2	Т	225 20	50	10" HG	1255 155	11.5		1036 - LB/HR ST 200 - LB/HR ST
L.O. SERV. (EMER)	2	М	225	50	5" HG	1200	10		
L.O. SERV. (MAIN)	2	RG	100	60/25	FLOODED	2179/726	11.5/.9		
JP-5 SERVICE JP-5 TRANSFER	1 1	R R	50 50	90 50	13" HG 13" HG	1800	4.0	5.0	

FEED, CONDENSATE &	NO. PER			DISCH PRESS	SUCTION		PUMP	MOTOR	
DRAIN PUMPS	SHIP	DRIVE	GPM	PSIG		RPM	ВНР	HP	REMARKS
MAIN FEED	4	T	240	789	50 FT. NPSH	6900	191		6384 LB/HR ST.
MAIN FEED BOOSTER	4	M	270	35	FLOODED	1785	8.5	10	
MAIN CONDENSATE	4	M	165	70	18" HG	1775	13.	20	
EMER. FEED & TRANSFER	2	RECIP	100	787	20" HG				9"x6"x16" SINGLE PISTON
SSTG COND CONDENSATE	4	M	40	7.5	4 FT	3550	4.8	5	
F.W. DRAIN TANK	2	M	30	50	0.5 FT	3500	3.75	5	
DIST SW HTR DRAIN	2	М	15	7.5	3 FT	3500	2.32	3	

DEAERATING FEED TANK		TEMPERATU	RE OF .	PRESSURE	AUX EXHAUST TO TANK		
NO. PER SHIP	CAPACITY, LB/HR	INLET	OUTLET	COND INLET	ST. INLET	SHELL	TU TANK
2	108,580	131	242	25	18		14,250

AUX AIR EJECTORS	NO. PER SHIP	TYPE	CAPACITY	REMARKS
SS TURBO-GEN COND		TWIN STAGE	9 LB/HR DRY AIR W/WATER VAP. AT 5" HG ABS. TEMP. AIR V. MIX. 121°F	138 LB/HR AT 135 PSIG AND 450-550°F
DISTILLING PLANT	2	TWO STAGE	39.5 LB/HR AIR W/WATER VAP. AT 2.99" HG BAS AND 105.8°F	475 LB/HR AT 135 PSIG AND 400°F

AIR CONDENSERS	NO. PER	TYPE	CAPACITY LB/HR	CIRC WATER GPM	COND V	AC ''HG	TEMP OF	CIRC WAT	ER ^O F	ST. TO COND LB/HR	AUX EXH TO COND LB/HR
SS TURBO-GEN COND		TWO PASS		875		5.0 ABS.		7.5	101.84	11,600	2000
AUX GLAND (LEAK OFF) CONDENSER	2	TWO PASS	300 AIR 1050 ST.	200	3"			85	97.1		

	NO. PER	LIO	UID	SURFACE	OIL FLOW	OIL TEM	MP OF	CIRC. WATER		
HEAT EXCHANGERS	SHIP	HEATED	COOLED	SQ FT	GPM	INLET	OUTLET	GPM	LB/HR	SW STEAM
L.O. COOLER	2			435	312 -	140	120	444		85
L.O. PUR. PRFGN PRE HTR WARM-UP	2			5.33	10 3.75	40	123 60		198 115	
THE THE STATE OF T										

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	RATINGS	OF	AUXILIARY	MACHINER'
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GLAND EXHAUSTER	NO. PER SHIP		CAPACITY, CF	M D	DISCH PRESS	SUCT. LIFT "H20	RPM	MOTOR HP
AUX. COND. GLAND	2	M	300		ATMOS ·		3500	3
Nox. Comp. Com.	1							

BLOWERS	NO. PER SHIP	DRIVE	CAPACITY (MAX	TOTAL HEAD	RPM	BHP	REMARKS
MAIN FORCED DRAFT	4	T	19,040SCFM	39.2" H ₂ 0	5010	177.2	
MAIN FORCED BRAIT		1					

	NO. PER		CAPA	CITY	AIR PRESS			THE RESERVE THE PARTY OF THE PA			
AIR COMPRESSORS		DRIVE	CFCA/HR	CFFA/MIN	DISCHARGE	SUCTION	DISCHARGE			BHP	MOTOR HP
SS AND CONTROL	4	М		100	150	ATMOS	100	122	830	27.06	30
										-	

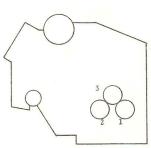
					The same of the sa					_	
GENERATORS	NO. PER	DRIVE	KW	VOLTS	PHASE	CYCLES	PF	AMPS	KVA	RPM	REMARKS
SSTURBO-GEN	4	T	1000	450	3	60	0.8	1602	1247	1200	ST AT 585 PSIG. 850°F, 9989
EMER. DIESEL	2	DIESEL	300	450	3	60	0.8	481	375	1800	

DISTILLING PLANT	TYPE	CAPACITY GPD	TOTAL STEAM CONSUMPTION	REMARKS
2 PER SHIP	L.P. 2 STAGE FLASH	30,000	5,325 LB/HR (HEATER) 475 LB/HR (EJECTOR)	426 GPM FEED

REFRIGERATION PLANT	NO. OF PLANTS PER SHIP	NO. OF COMPRESSORS PER SHIP	CAPACITY PER COMPRESSOR, TONS	MOTOR H.P.	-
AIR CONDITIONING	4	4	65	75	onderen.
SHIPS STORES	1	2	22.8	30	

BOILER	OPERATION
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	And the state of t	0 SHP	
		0 RPM	
M	AIN STEAM CONDITIONS DRUM PRESSURE. SUPERHEATER OUTLET PRESSURE. SUPERHEATER OUTLET TEMPERATURE.	660 PSIG 660 PSIG 855° F	
A	UXILIARY STEAM CONDITIONS DESUPERHEATER OUTLET PRESSURE DESUPERHEATER OUTLET TEMPERATURE	660 PSIG 515° F	
N B	UMBER OF BOILERS IN USE UMBER OF BURNERS IN USE PER BOILERurner TIP SIZE.		
F	UEL OIL PER BURNER. UEL OIL TOTAL (SHIP). UEL OIL SERVICE DISCHARGE PRESSURE. UEL OIL PRESSURE (BURNER HEADER).	400 PSIG	
F A C T	UMBER OF BLOWERS IN USE PER BOILER. ORCED DRAFT BLOWER SPEED (ESTIMATED) IR PRESSURE AT FORCED DRAFT BLOWER DISCHARGE IR PRESSURE AT BOILER FRONT CASING. O, IN STACK GAS. URBO GENERATOR LOAD (ESTIMATED)	7.2 IN. H ₂ 0 5.2 IN. H ₂ 0 13.5% 1243 KW	
A	UXILIARY EXHAUST MAIN PRESSURE	15 PSIG	
	EEDWATER TEMPERATURE (ECONOMIZER OUTLET)	333°F	



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BOILER OPERATION

STANDBY ONE BOILER	0 SHP 0 RPM	
MAIN STEAM CONDITIONS DRUM PRESSURE. SUPERHEATER OUTLET PRESSURE. SUPERHEATER OUTLET TEMPERATURE.	660 PSIG	
AUXILIARY STEAM CONDITIONS DESUPERHEATER OUTLET PRESSURE DESUPERHEATER OUTLET TEMPERATURE	660 PSIG 515°F	
NUMBER OF BOILERS IN USE NUMBER OF BURNERS IN USE PER BOILER BURNER TIP SIZE	1	
FUEL OIL PER BURNER. FUEL OIL TOTAL (SHIP). FUEL OIL SERVICE DISCHARGE PRESSURE.	2152 LB/HR	(
FUEL OIL PRESSURE (BURNER HEADER)	225 PSIG	
NUMBER OF BLOWERS IN USE PER BOILER. FORCED DRAFT BLOWER SPEED (ESTIMATED) AIR PRESSURE AT FORCED DRAFT BLOWER DISCHARGE AIR PRESSURE AT BOILER FRONT CASING. CO, IN STACK GAS TURBO-GENERATOR LOAD (ESTIMATED)	2150 RPM 8.8 IN. H ₂ 0 6.5 IN. H ₂ 0 13.9%	LQ
AUXILIARY EXHAUST MAIN PRESSURE	15 PSIG	
FEEDWATER TEMPERATURE (ECONOMIZER OUTLET)	3330F 245 ^o F	

STANDBY TWO BOILERS	0 SHP 0 RPM
MAIN STEAM CONDITIONS DRUM PRESSURE. SUPERHEATER OUTLET PRESSURE. SUPERHEATER OUTLET TEMPERATURE.	000 P31G
AUXILIARY STEAM CONDITIONS DESUPERHEATER OUTLET PRESSURE DESUPERHEATER OUTLET TEMPERATURE	660 PSIG 515°F
NUMBER OF BOILERS IN USE NUMBER OF BURNERS IN USE PER BOILER BURNER TIP SIZE	
FUEL OIL PER BURNER FUEL OIL TOTAL (SHIP) FUEL OIL SERVICE DISCHARGE PRESSURE	3004 LD/III
FUEL OIL PRESSURE (BURNER HEADER)	110 PSIG
NUMBER OF BLOWERS IN USE PER BOILER. FORCED DRAFT BLOWER SPEED (ESTIMATED). AIR PRESSURE AT FORCED DRAFT BLOWER DISCHARGE. AIR PRESSURE AT BOILER FRONT CASING. CO ₂ IN STACK GAS. TURBO-GENERATOR LOAD (ESTIMATED).	
AUXILIARY EXHAUST MAIN PRESSURE	15 PSIG
FEEDWATER TEMPERATURE (ECONOMIZER OUTLET). FEEDWATER TEMPERATURE (DFT OUTLET)	333°F 245°F

20 KNOTS ENDURANCE	18300 RPM 216 RPM
DRUM PRESSURE.	660 PSIG 660 PSIG 855°F
	600 PSIG 580°F
NUMBER OF BOILERS IN USE. NUMBER OF BURNERS IN USE PER BOILER. BURNER TIP SIZE.	5-41-53-53-80
FUEL OIL PER BURNER FUEL OIL TOTAL (SHIP). FUEL OIL SERVICE DISCHARGE PRESSURE.	8
FUEL OIL PRESSURE (BURNER HEADER)	210 PSIG
NUMBER OF BLOWERS IN USE PER BOILER. FORCED DRAFT BLOWER SPEED (ESTIMATED). AIR PRESSURE AT FORCED DRAFT BLOWER DISCHARGE. AIR PRESSURE AT BOILER FRONT CASING. CO ₂ IN STACK GAS. TURBO-GENERATOR LOAD (ESTIMATED).	14.2 IN. H ₂ 0 11.5 IN. H ₂ 0 13.9%
AUXILIARY EXHAUST MAIN PRESSURE	
FEEDWATER TEMPERATURE (ECONOMIZER OUTLET)	350°F 245°F

FULL POWER	24000 SHP 235 RPM		
MAIN STEAM CONDITIONS DRUM PRESSURE. SUPERHEATER OUTLET PRESSURE. SUPERHEATER OUTLET TEMPERATURE.	600 PSIG		
AUXILIARY STEAM CONDITIONS DESUPERHEATER OUTLET PRESSURE DESUPERHEATER OUTLET TEMPERATURE.	570 PSIG 588°F		
NUMBER OF BOILERS IN USE NUMBER OF BURNERS IN USE PER BOILER BURNER TIP SIZE	3		
FUEL OIL PER BURNER. FUEL OIL TOTAL (SHIP). FUEL OIL SERVICE DISCHARGE PRESSURE.	15864 LB/HR	(
FUEL OIL PRESSURE (BURNER HEADER)	320 PSIG		
NUMBER OF BLOWERS IN USE PER BOILER. FORCED DRAFT BLOWER SPEED (ESTIMATED) AIR PRESSURE AT FORCED DRAFT BLOWER DISCHARGE AIR PRESSURE AT BOILER FRONT CASING. CO ₂ IN STACK GAS TURBO-GENERATOR LOAD (ESTIMATED).	4300 RPM 25 IN. H ₂ 0 14.5 IN. H ₂ 0 13.9%		3
AUXILIARY EXHAUST MAIN PRESSURE	15 PSIG		
FEEDWATER TEMPERATURE (ECONOMIZER OUTLET)FEEDWATER TEMPERATURE (DFT OUTLET)	335°F 245°F		

	ASTERN	4800 SHP 130 RPM
	MAIN STEAM CONDITIONS DRUM PRESSURE. SUPERHEATER OUTLET PRESSURE. SUPERHEATER OUTLET TEMPERATURE.	· 625 PS16
	AUXILIARY STEAM CONDITIONS DESUPERHEATER OUTLET PRESSURE DESUPERHEATER OUTLET TEMPERATURE	600 PSIG 583°F
	NUMBER OF BOILERS IN USE	3
	FUEL OIL PER BURNER. FUEL OIL TOTAL (SHIP). FUEL OIL SERVICE DISCHARGE PRESSURE.	1140/ LB/RK /
18	FUEL OIL PRESSURE (BURNER HEADER)	180 PSIG
	NUMBER OF BLOWERS IN USE PER BOILER. FORCED DRAFT BLOWER SPEED (ESTIMATED). AIR PRESSURE AT FORCED DRAFT BLOWER DISCHARGE. AIR PRESSURE AT BOILER FRONT CASING. CO, IN STACK GAS. TURBO-GEMERATOR LOAD (ESTIMATED)	2800 RPM 13.6 IN. H ₂ 0 9.7 IN. H ₂ 0
	AUXILIARY EXHAUST MAIN PRESSURE	·· 15 PSIG
	FEEDWATER TEMPERATURE (ECONOMIZER OUTLET)	3500F 2450F

PROPULSION TURBINE OPERATING CONDITIONS PER SHAFT

	PROPULSION TURB	INE OPERATING CONL			
SPEED OF SHIP		20 KNOTS	FULL POWER	ASTERN	OVERLOAD
SHAFT HORSEPOWER SHAFT REVOLUTION	SHP RPM	9150 216	12000 235	2400 130	11800 187,5
THROTTLE STEAM PRESSURE THROTTLE STEAM TEMPERATURE THROTTLE STEAM FLOW LB/HR STEAM RATE LB/SHAFT HP/HR	PSIG °F	615 860 53370 6.27	585 850 77280 6.44	615 860 53760 22.4	575 840 77499 6.57
HP TURBINE HP TURBINE SHAFT HORSEPOWER LP TURBINE LP TURBINE SHAFT HORSEPOWER LP TURBINE MOISTURE \$ AHEAD NOZZLE AREA ACTION SQ. IN.	RPM SHP RPM SHP	7019 4950 4870 4200 9.0 2.54	7637 6000 5298 6000 8.6 3.39	2-	6009 3380 4220 2520 8.5 1.905
HP TURBINE INLET PRESSURE HP TURBINE INLET TEMPERATÜRE HP TURBINE EXHAUST PRESSURE HP TURBINE EXHAUST TEMPERATURE	PSIG OF PSIA OF	615 860 34.6 333	585 850 45.4 369	615 860 	575 840 17 245
LP TURBINE INLET PRESSURE LP TURBINE INLET TEMPERATURE LP TURBINE EXHAUST PRESSURE LP TURBINE EXHAUST TEMPERATURE	PSIA of PSIA oF	33.6 333. .835 96	44.4 369 .98 101	 	16 243 .72 90.8
ASTERN TURBINE INLET PRESSURE ASTERN TURBINE INLET TEMPERATURE ASTERN TURBINE EXHAUST PRESSURE ASTERN TURBINE EXHAUST TEMPERATURE	PSIG OF PSIA OF	1		395 845 1.47 556	
MAIN CONDENSER EXHAUST PRESSURE IN. HG AI	BS	1.7	2.0	3.0	1.4

PROPULSION AUXILIARY MACHINERY IN USE

		TOT OLUTONIE	Dati milotimani in con			
	PLANT CONDITION SHIPS SPEED KNOTS	PORT AT ANCHOR	20 KNOTS	SPLIT PLANT FULL POWER	AS TERN	X C ONN 20% OV LD
NO. PER SHIP	IDENTIFICATIONS		Q	TY IN USE PER SHII	D -	
2	BOILERS	1	2	2	2	SEE NOTE 1
4T	MAIN FEED PUMP	1	2	4	2	2
4 M	MAIN FEED BOOSTER PUMP · · · · · · · · · · · · · · · · · · ·	1	2	4	2	2
2R	EMERGENCY FEED PUMP	0	0	0	0	0
2	DEAERATING FEED HEATER	1	2	2	2	1
4 T	MAIN FORCED DRAFT BLOWER	1	4	4	4	2
4T	MAIN FUEL OIL SERVICE PUMP	0	2	2	2	1
2M	PORT USE FUEL OIL SERVICE PUMP	1	0	0	0	0
2	FEED WATER COOLER	1	2	2	2	1
	M-MOTOR DRIVER	N .	R - RECIPROCATI	NG	T - TURBINE	DRIVEN

NOTE 1 - DURING 20% OVERLOAD, BOILER IN NO. L MACHINERY SPACE SHALL BE PLACED IN OPERATION.

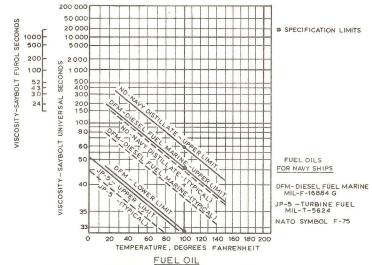
PROPULSION AUXILIARY MACHINERY IN USE

	SHIPS SPEED KNOTS	PORT AT NCHOR	SPLIT PLANT 20 FULL KNOTS POWER	ASTERN	X C ONN 2 0% OV LD
NO.PER SHIP	IDENTIFICATIONS		QTY IN USE PER SHIP		
2	MAIN PROPULSION TURBINE SETS	0	, 2 ,	2	2
4 M	MAIN CONDENSATE PUMP	0	2 4	2	2
2	MAIN AIR EJECTOR	0	2 2	2	2
2M	MAIN CIRCULATING PUMP	0	0 0	2	0
2M	MAIN LO SERVICE PUMP (EMERGENCY)		EMERGENCY STANDBY		
2T	MAIN LO SERVICE PUMP (STANDBY)	0	2- IDLING IDLING	2	2- IDLING
2	ATTACHED LO SERVICE PUMP	0	2 2	0	2
2	LUBE OIL COOLER		2 2	2	2
4	TURBO-GENERATORS		2 2	2	2
	TURBO-GENERATOR CONDENSATE PUMP	2	2 2	2	2
4M	TURBO-GENERATOR CIRCULATING PUMP	2	2 2	2	2
4M	TURBO-GENERATOR CIRCULATING FORM:		2 2	2	2
4	AUXILIARY GLAND LEAKOFF CONDENSER		2 2	2	2

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BOILER OPERATING DATA (USING DISTILLATE FUEL)

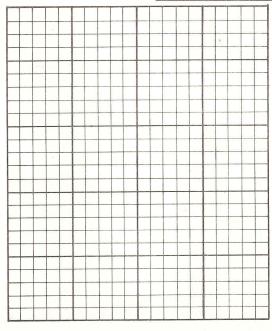
. ALMOST ALL NAVAL BOILERS HAVING UNCONTROLLED SUPERHEATERS CAN ANTICIPATE SOME INCREASE IN SUPERHEATER OUTLET STEAM TEMPERATURE AFTER CONVERTING TO DISTILLATE FUEL. THE MAXIMUM LIMIT IS 850°F UNDER STEADY STATE CONDITIONS. BRIEF EXCURSIONS ABOVE THIS TEMPERATURE ARE TO BE EXPECTED DURING BOILER LOAD CHANGES.

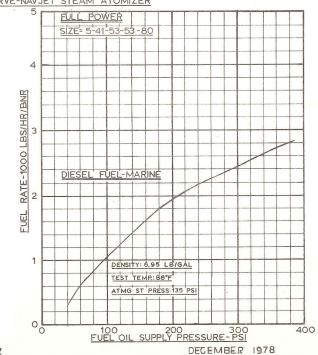


FUEL OIL TEMPERATURE - VISCOSITY CHART

21







22

SAFETY PRECAUTIONS

- 1. PIPING JOINTS MUST BE MAINTAINED TIGHT AND VALVES KEPT IN GOOD WORKING ORDER AT ALL TIMES.
- 2 NEVER ATTEMPT TO TIGHTEN A PRESSURIZED PIPING JOINT OR LEAKING COMPONENT BY SHARP OR HEAVY BLOWS OR APPLICATION OF HEAT. SUCH ACTION CAN RESULT IN SUDDEN FAILURE OF PRESSURIZED PIPING, OR AN EXPLOSION OF THE SYSTEM.
- 3. NEVER DEACTIVATE OR BYPASS A SAFETY DEVICE.

 4. ALL WATER FROM STEAM PIPING SHOULD BE DRAINED BEFORE OPENING LINE VALVES TO PREVENT WATER HAMMER AND POSSIBLE DAMAGE TO PIPING AND EQUIPMENT. THE VALVE BYPASS ON LARGE STEAM VALVES TO WARM UP
 - MUST BE OPENED BEFORE OPENING THE MAIN LINE VALVE TO WARM UP THE LINE AND EQUALIZE THE PRESSURES. IF BYPASSES ARE NOT IN-STALLED THE VALVES SHOULD BE OPENED SLOWLY.
- 5, ALL STEAM GLOBE, GATE AND ANGLE VALVES AND MANY VALVES USED IN OTHER SYSTEMS ARE EQUIPPED WITH BACK SEATS. A BACK SEAT IN GOOD CONDITION WILL REMOVE PRESSURE FROM THE PACKING GLAND WHEN THE VALVE IS FULLY OPEN. TO PROLONG THE LIFE OF PACKING, AND MINIMIZE CHANCE OF LEAKAGE OR BLOWING PACKING FROM VALVE GLANDS, ALL VALVES ARE TO BE FULLY OPEN OR FULLY CLOSED EXCEPT WHEN ACTUALLY BEING USED FOR THROTTLING PURPOSES. NORMAL HANDWHEEL TORQUE IS TO BE USED FOR SEATING AND BACKSEATING THE VALVE. NO WRENCH OR OTHER TOOL SHOULD BE NEEDED TO OPEN OR CLOSE A PROPERLY MAINTAINED VALVE.
- 6.IN CASE OF FIRE IN THE BILGES, CLOSE THE FUEL OIL CUTOUT VALVE AND STOP THE FUEL OIL PUMP. EXTINGUISH THE FIRE WITH PKP AND/
- 7. IN CASE OF FIRE IN THE BOILER CASING, STOP THE FUEL SUPPLY TO THE BURNERS, STOP THE FUEL OIL PUMP, AND IMMEDIATELY ADMIT SMOTHERING STEAM TO THE CASING.
- 8.IN CASE OF MACHINERY BREAKDOWN, LOCATE THE CAUSE OF THE TROUBLE AND NOTIFY THE OFFICER OF THE WATCH.
- 9. OPERATING PERS ONNEL SHOULD THOROUGHLY FAMILIARIZE THEMSELVES WITH THE SYSTEMS ABOARD SHIP BY ACTUALLY TRACING OUT INDIVIDUAL LINES AND EQUIPMENT.
- 10.CLEAN ALL STRAINERS PERIODICALLY AS REQUIRED IN ACCORDANCE WITH PREVENTIVE MAINTENANCE SYSTEM.

- 11.ALL SOUNDING TUBE CAPS SHOULD BE TIGHTLY SECURED WHEN NOT IN ACTUAL USE.
- 12. FREQUENT INSPECTIONS SHALL BE MADE TO ENSURE THAT FLASH SCREENS IN VENTS FROM FUEL TANKS ARE INTACT AND CLEAN ESPECIALLY AFTER PAINT SPRAYING IN VICINITY OF THE VENT TERMINALS IN ACCORDANCE WITH PREVENTIVE MAINTENANCE SYSTEM.
- 13 AUTOMATIC AIR RELIEF VALVES OR PRESSURE-VACUUM RELIEF VALVES
 FITTED TO THE TANKS OR IN THE TANK VENT SYSTEM SHALL BE TRIED
 FREQUENTLY FOR FREE OPERATION AND ONCE DURING EACH QUARTER
 SHALL BE THOR QUICHLY INSPECTED AND CLEANED.
- SHALL BE THOROUGHLY INSPECTED AND CLEANED.

 14. USE CO2 OR PKP, IF CO2 IS NOT READILY AVAILABLE, TO EXTINGUISH AN ELECTRICAL FIRE. DO NOT USE WATER.
- 15 . FOR MOTOR OPERATED EQUIPMENT
 - A .BEFORE STARTING WORK ON UNIT OPEN AND TAG APPLICABLE MANUAL OR AUTOMATIC SWITCH OR CONTROLLER TO DEENERGIZE SYSTEM.
 - B.BEFORE STARTING ELECTRICAL REPAIR LOCK APPLICABLE CIRCUIT BREAKER IN "OFF" POSITION AND ATTACH WARNING TAG.
 - C.REFER TO CHAPTER 300 NAVSEA TECHNICAL MANUAL FOR ADDI-TIONAL SAFETY PRECAUTIONS.

16 FOR STEAM DRIVEN PUMPS

- A.DO NOT TIE DOWN, OR OTHERWISE RENDER INOPERATIVE, THE OVER-SPEED TRIP, SPEEDLIMITING OR SPEED-REGULATING GOVERNORS.
- B.CHECK THE SETTING OF OVERSPEED TRIP, SPEEDLIMITING AND SPEED-REGULATING GOVERNORS AT LEAST QUARTERLY.
- C.BEFORE STARTING REPAIR OPERATIONS ON THE UNIT, WIRE CLOSE AND TAG THE STEAM SUPPLY VALVE, OIL SUCTION AND DISCHARGE VALVES.
- D.REFER TO CHAPTER 503 NAVSEA TECHNICAL MANUAL FOR ADDITIONAL SAFETY PRECAUTIONS.

SAFETY PRECAUTIONS WHEN OPERATING WITH DISTILLATE FUEL 1. KEEP FIRE FIGHTING EQUIPMENT IN GOOD WORKING CONDITION AND READILY ACCESSIBLE. SMOKE IN THE POSTED SAFE AREAS ONLY. WIPE UP SPILLED OIL AT ONCE.

2. CAREFUL HANDLING OF TORCH AND TORCH POT IS MANDATORY TO PREVENT THE POSSIBILITY OF OIL SPILLAGE AND FIRE.

3.WHEN, LIGHTING OFF A BURNER, TWO MEN ARE REQUIRED; ONE MAN TO OPERATE AIR REGISTER AND INSERT TORCH; AND ANOTHER TO OPERATE FUEL OIL HEADER TOOT VALVES. DO NOT ATTEMPT TO RELIGHT FIRES

OFF HOT BRICKWORK. 4 SHOULD LEAKAGE FROM THE FUEL OIL SYSTEM INTO THE FIRE ROOM OCCUR AT ANY TIME, IMMEDIATELY SECURE THE FUEL OIL SUPPLY BY MEANS OF THE QUICK CLOSING VALVES AND STOP THE FUEL OIL PUMP.

- 5. DISTILLATE FUEL WILL PRODUCE GASEOUS VAPORS AT TEMPERATURES APPROXIMATELY \pm 135°F. THESE VAPORS, WHEN MIXED IN THE PROPER PROPORTIONS WITH AIR, ARE EASILY IGNITED AND, IN SOME CASES CAN BE EXPLOSIVE. THUS, IT IS IMPORTANT TO PREVENT UNBURNED OIL FROM ACCUMULATING AND VAPORIZING. FREQUENT INSPECTIONS FOR LEAKS, SPILLAGE AND COLLECTED POOLS IS REQUIRED TO PREVENT
- 6. OIL VAPORS ARE HEAVIER THAN AIR AND WILL TEND TO ACCUMULATE IN LOWER LEVELS SUCH AS BILGES. IGNITION OF THIS TYPE OF EX-PLOSIVE MIXTURE MAY BE EASILY CAUSED BY OPEN FLAMES SMOKING TOBACCO, ELECTRIC OR METALLIC SPARKS, HOT LAMP FILA-MENTS OR HOT METAL SURFACES. OIL VAPOR EXPLOSIONS ARE USUALLY FOLLOWED BY FIRE WHEN OIL AND/OR COMBUSTIBLE MATERIALS ARE

7. IN TAKING ACTION TO EXTINGUISH AN OIL FIRE, PKP WITH A BLANKET OF AFFF, OR STEAM SMOTHERING (INSIDE BOILER CASING), ARE MOST EF-FECTIVE. IT MAY BE NECESSARY TO EVACUATE PERSONNEL AND SECURE ALL OPENINGS TO THE SPACE.

8. INSPECT ALL STORAGE TANKS IN ACCORDANCE WITH PREVENTIVE MAIN-TENANCE SYSTEM.

9. PORTABLE COMBUSTIBLE GAS INDICATING INSTRUMENTS FOR DETECTING THE PRESENCE OF HYDROCARBON VAPORS AND OTHER COMBUSTIBLE GASES ARE AVAILABLE AND ARE IN THE SHIP'S ALLOWANCE LIST. THESE INSTRUMENTS SHOULD BE USED FOR DETECTING VAPORS IN SPACES INTO WHICH FUEL MIGHT LEAK OR IN WHICH THE PRESENCE OF HYDROCARBON VAPORS OR OTHER COMBUSTIBLE GASES ARE SUSPECTED.

SAFETY PRECAUTIONS ASSOCIATED WITH COMPRESSED AIR SYSTEMS 1. NEVER USE ANY FLAMMABLE SOLVENTS, OR VOLATILE OILS, TO CLEAN COMPRESSOR INTAKE AIR FILTERS, VALVES, CYLINDERS OR AIR PASSAGES. THESE LIQUIDS VAPORIZE EASILY AND WILL FORM EXPLOSIVE AIR/OIL MIXTURES WHEN COMPRESSED.

2. NEVER ATTEMPT TO TIGHTEN A PRESSURIZED PIPING JOINT OR LEAKING COMPONENT BY SHARP OR HEAVY BLOWS OR APPLICATION OF HEAT. SUCH ACTION CAN RESULT IN SUDDEN FAILURE OF PRESSURED PIPING OR AN EXPLOSION OF THE SYSTEM.

3. SECURE AN AIR COMPRESS OR IMMEDIATELY IF NOT SPOTS ARE DETER-MINED BY TOUCH, OR IF THE DISCHARGE TEMPERATURE FROM ANY STAGE RISES UNDULY, OR EXCEEDS 400°F, INVESTIGATE AND DETERMINE THE CAUSE SINCE EXCESSIVE TEMPERATURES CAN RESULT IN AUTO-IGNITION.

4.DO NOT ATTEMPT TO RESTART AN AIR-COMPRESSOR AFTER SHUT-DOWN BY AN AUTOMATIC SAFETY DEVICE UNTIL THE CAUSE OF THE SHUT-DOWN HAS BEEN DETERMINED AND CORRECTED. FAILURE TO COMPLY WITH THIS INSTRUCTION MAY CAUSE SERIOUS DAMAGE TO THE EQUIPMENT AND/ OR INJURY TO OPERATING PERSONNEL.

5. HIGH PRESSURE AIR VALVES SHOULD BE SLOWLY CRACKED OPEN UNTIL FLOW IS NOTED, AND SHOULD REMAIN IN THIS POSITION UNTIL THE PRES-SURES ON BOTH SIDES HAVE GRADUALLY EQUALIZED. THE RATE OF AIR PRESSURE RISE SHOULD NOT EXCEED 200 PSI PER SECOND.

6. BEFORE WORKING ON A HIGH PRESSURE COMPRESSED AIR SYSTEM: A. SECURE AIR COMPRESSOR. OPEN AND TAG CIRCUIT BREAKER. B. BLOW-DOWN SYSTEM COMPLETELY.

C. CLOSE ALL SYSTEM VALVES AND TAG SHUT IS OLATION VALVES. D. OBSERVE GAGES FOR INDICATIONS OF REMAINING AIR PRESSURES.

7. IF ANY OF THE AIR COMPRESSORS ARE TO REMAIN IDLE FOR SEVERAL WEEKS, IT IS RECOMMENDED THAT THE IDLE UNITS BE OPERATED FOR ABOUT A HALF HOUR EACH WEEK. THIS OPERATION WILL KEEP THE COM-PRESS OR WELL LUBRICATED TO PREVENT CORROSION AND WILL ENSURE THAT THE CONTROL EQUIPMENT IS IN GOOD OPERATING CONDITION.

8. IF THE EQUIPMENT IS TO REMAIN IDLE FOR LONGER PERIODS WITHOUT BE-ING OPERATED, THE IDLE EQUIPMENT MAINTENANCE PROCEDURES LISTED IN THE MANUFACTURERS TECHNICAL MANUAL SHOULD BE FOLLOWED.

